



**Fig. 12.1** • Cohesive powder poured in a heap and showing different angles of repose:  $\theta_m$  maximum angle formed by cohesive particles  $\theta_s$  shallowest angle formed by collapse of cohesive particle heap, resulting in flooding. In some cases, a third angle,  $\theta_i$  is identifiable as an intermediate slope produced by cohesive particles stacking on flooded powder.

mobile. The resulting heap has two angles of repose: a large angle remaining from the initial heap and a shallower angle formed by the powder flooding from the initial heap (Fig. 12.1).

## Particle properties and bulk flow

In the discussion concerning adhesion/cohesion it is clear that an equilibrium exists between forces responsible for promoting powder flow and those preventing powder flow, i.e. at equilibrium:

$$\Sigma f(\text{driving forces}) = \Sigma f(\text{drag forces}) \quad (12.1)$$

that is:

$$\Sigma f(\text{gravitational force, particle mass, angle of inclination of powder bed, static head of powder, mechanical force...}) = \Sigma f(\text{adhesive forces, cohesive forces, other surface forces, mechanical interlocking...}) \quad (12.2)$$

Some of these forces are modified or controlled by external factors related to particle properties, such as size, shape and density.

### Particle size effects

Because adhesion and cohesion are phenomena that occur at surfaces, particle size will influence the flowability of a powder. In general, fine particles

with very high surface-to-mass ratios are more adhesive/cohesive than coarser particles which are influenced more by gravitational forces. Particles larger than 250  $\mu\text{m}$  are usually relatively free flowing but as the size falls below 100  $\mu\text{m}$ , powders become more adhesive/cohesive and flow problems are likely to occur. Powders having a particle size less than 10  $\mu\text{m}$  are usually extremely adhesive/cohesive and resist flow under gravity. An important exception to this reduction in flowability is when the very small particles become adhered/cohered to larger ones and the flowability of the powder as a whole then become controlled by the larger particles. This phenomenon is important in the concept of ordered mixing (Chapter 11) and formulation of dry powder inhalers (Chapter 37).

### Particle shape

Powders with similar particle sizes but dissimilar shapes can have markedly different flow properties owing to differences in interparticulate contact areas. For example, a group of spheres has minimum interparticulate contact and generally optimal flow properties, whereas a group of particle flakes or dendritic particles has a very high surface-to-volume ratio and poorer flow properties. Irregular shaped particles may experience mechanical interlocking in addition to adhesional and cohesive forces.

### Particle density (true density)

Because powders normally flow under the influence of gravity, higher density particles are generally less adhesive/cohesive than less dense particles of the same size and shape.

## Packing geometry

A set of particles can be filled into a volume of space to produce a powder bed which is in static equilibrium owing to the interaction of gravitational and adhesive/cohesive forces. By slight vibration of the bed, particles can be mobilized so that if the vibration is stopped, the bed is once more in static equilibrium but occupies a different spatial volume than before. The change in bulk volume has been produced by rearrangement of the packing geometry of the particles. In general, such geometric rearrangements result in a transition from loosely packed particles to more tightly packed ones, so that the